## **CLAIMS**

## There is claimed:

- 1. A process for the continuous production of coke, which comprises:

  (a) providing a means for heating petroleum residuum to a temperature within the range from about 850 1000 degree F., (b) transferring the resulting heated petroleum residuum to a vessel, (c) releasing of vapors within said vessel, (d) wherein the residence time of the remaining petroleum residuum is less than 5 minutes within said vessel, transferring the remaining petroleum residuum from near the bottom of said vessel to a reactor vessel, (e) operating said reactor vessel under pressure ranging from about 4 psia to 65 psia, (f) mixing and kneading within said reactor vessel to promote devolatilization, carbonization and formation of coke, (g) providing a means for cooling the resulting coke product to a range from about 100 250 degrees F and (h) transporting the resulting coke.
- 2. The process of claim 1 wherein the mixing and kneading step occurs by using a reactor vessel with a single agitation shaft and with an inlet for the remaining petroleum residuum and an outlet for the resulting coke product, and multi-vapor outlets.
- 3. The process of claim 1 wherein the mixing and kneading step occurs by using a reactor vessel with multiple agitation shafts, including a main agitator shaft and a cleaning agitator shaft, so that the shafts continuously scrape the resulting coke from the reactor as well as from each of the agitation shafts.
- 4. The process of claim 1 wherein an amount of air or oxygen may be added to said reactor vessel thereby increasing the temperature and hence the rate of cracking reactions and carbonization reactions.
- 5. The process of claim 1 wherein the means for cooling the resulting coke is provided with either air or closed circuit cooling water.
- 6. The process of claim 1 wherein the means for cooling the resulting coke is provided by applying water directly to the resulting coke and forming a coke slurry.